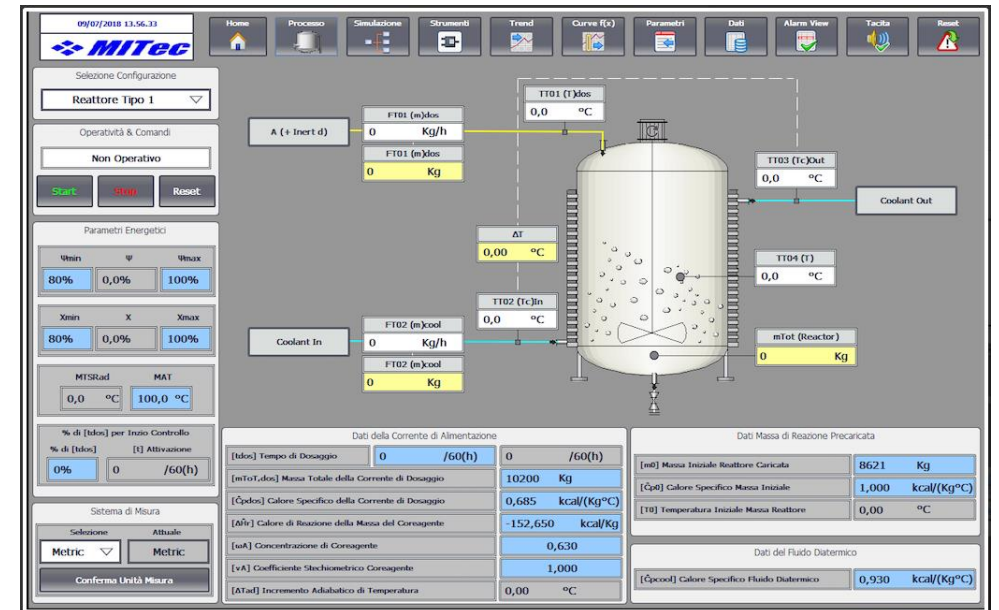


# Selection and Monitoring of Safe and Productive Operating Conditions for Discontinuous Runaway Reactions: the Energy Release Monitoring System (ERMES) Method

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Processes with Hazardous Chemicals  
Practical Learnings



# Runaway reactions: a long list of catastrophes



Phenolic resins, Italy 1997



Acrylic polymers, N.C. - USA 2006



Gasoline additives, FL - USA 2007

# Introductory concepts

## Fast and exothermic reactions: possible incidental scenarios

**Thermal explosion:** final consequence of the unbalance between heat generation by the chemical reaction and heat removal by the reactor cooling system.

**Thermal runaway:** triggering of a consecutive decomposition of the reaction mass with sudden generation of permanent gases within a confined space (reaction vessel).

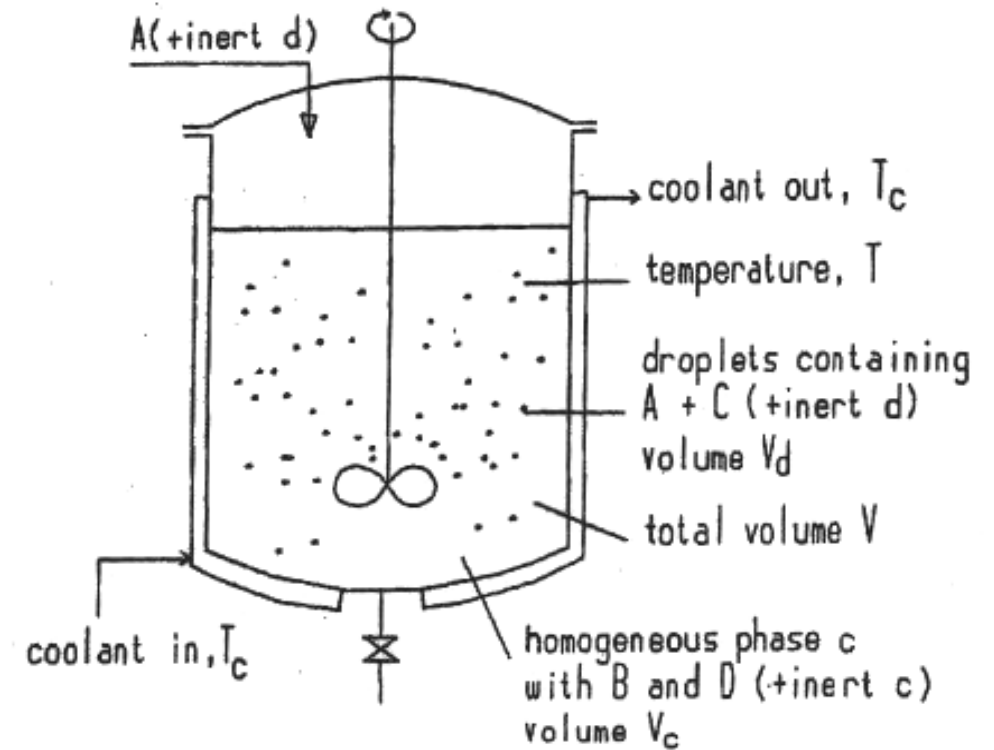
Both the phenomena can generate a dangerous reactor overpressure:

- ❖ as a consequence of the *reaction mass vapor pressure* → **vapor pressure systems;**
- ❖ as a consequence of the *reaction mass decomposition* → **gassy systems.**

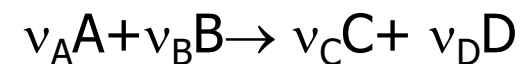


# Reactor selection

- ❖ A number of reaction processes of this type can be found in the *fine chemical and pharmaceutical industries* and are therefore performed in *non-continuous multipurpose reactors (batch, BR, or semibatch, SBR)*;
- ❖ When a thermal loss of control of the reaction can occur, the choice of a *semibatch reactor (SBR)* is strongly recommended (that is, one reactant initially loaded and one reactant dosed in a suitable time period).
- ❖ This allows for **controlling the conversion rate and the reaction heat evolution.**



Chemical reaction:



# Mathematical model

## Macroscopic mass and energy balances:

$$\begin{aligned} \frac{dn_i}{dt} &= F_{i,dos} + v_i r^{eff} V_r && \text{Reaction macrokinetics} \\ (n\tilde{C}_P) \frac{dT}{dt} &= (-\Delta\tilde{H}_r) r^{eff} V_r - \left[ (F\tilde{C}_P)_{dos} (T - T_{dos}) + UA(T - \bar{T}_{cool}) \right] \\ &&& \text{Reaction Enthalpy contribution} \quad \text{Combined cooling contribution} \end{aligned}$$

However, at the industrial scale:

- ❖ The **system modeling** is **not always feasible** for time and resources constraints (often when dealing with multipurpose processes);
- ❖ The **reaction macrokinetics** is **often unknown**.

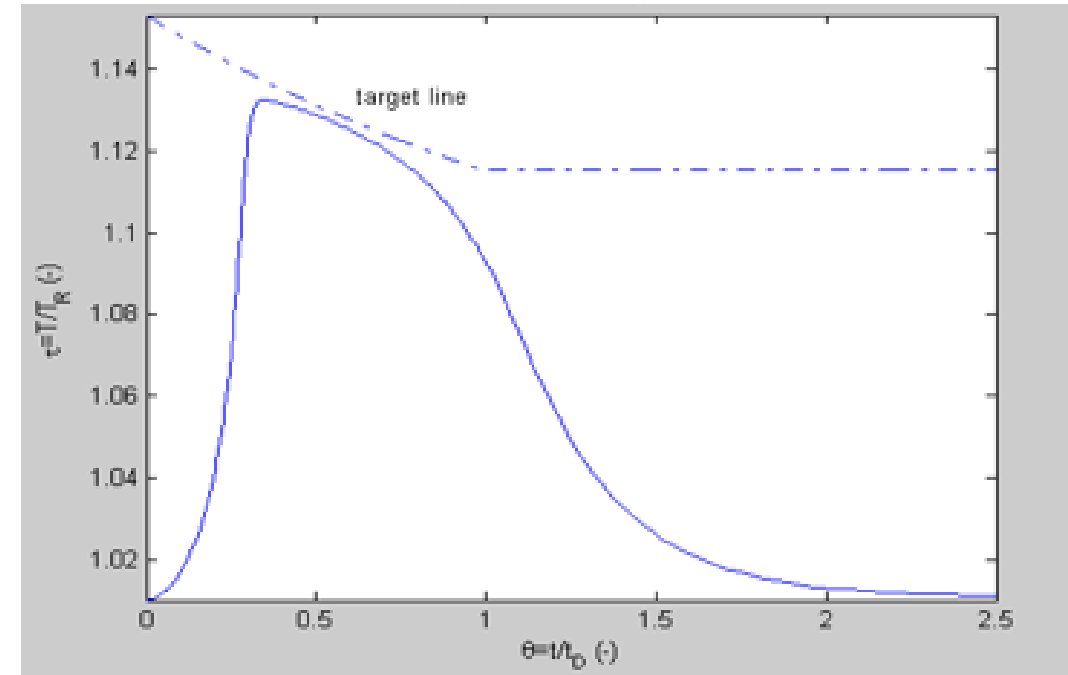
# Target operating conditions

Definition and monitoring of a *set of safe and productive operating conditions of the SBR* through:

- ❖ *Effective limitation of the dosed reactant accumulation in the SBR* → conversion rate  $\cong$  dosing rate (**kinetic-free conditions**);
- ❖ *Effective removal of the reaction heat* → nearly isothermal SBR operation.

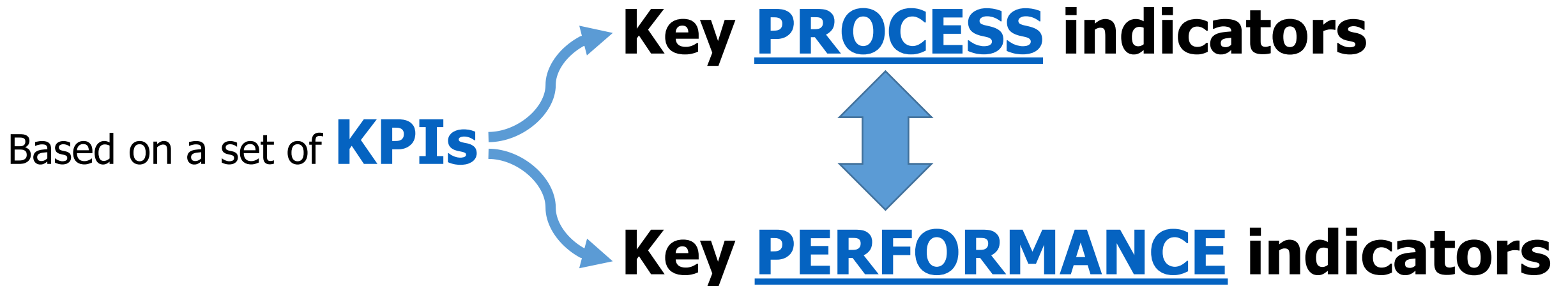
Such a regime is achieved adopting a suitable **dosing time** of the fed reactant, which has to be:

- ❖ *Enough high* to allow for a *safe SBR operation*;
- ❖ *Enough low* to allow for a *satisfactory SBR productivity*.



**A reaction inhibition during the dosing period and/or an early decay of the heat removal efficiency are root causes of dangerous scenarios**

# The ERMES approach



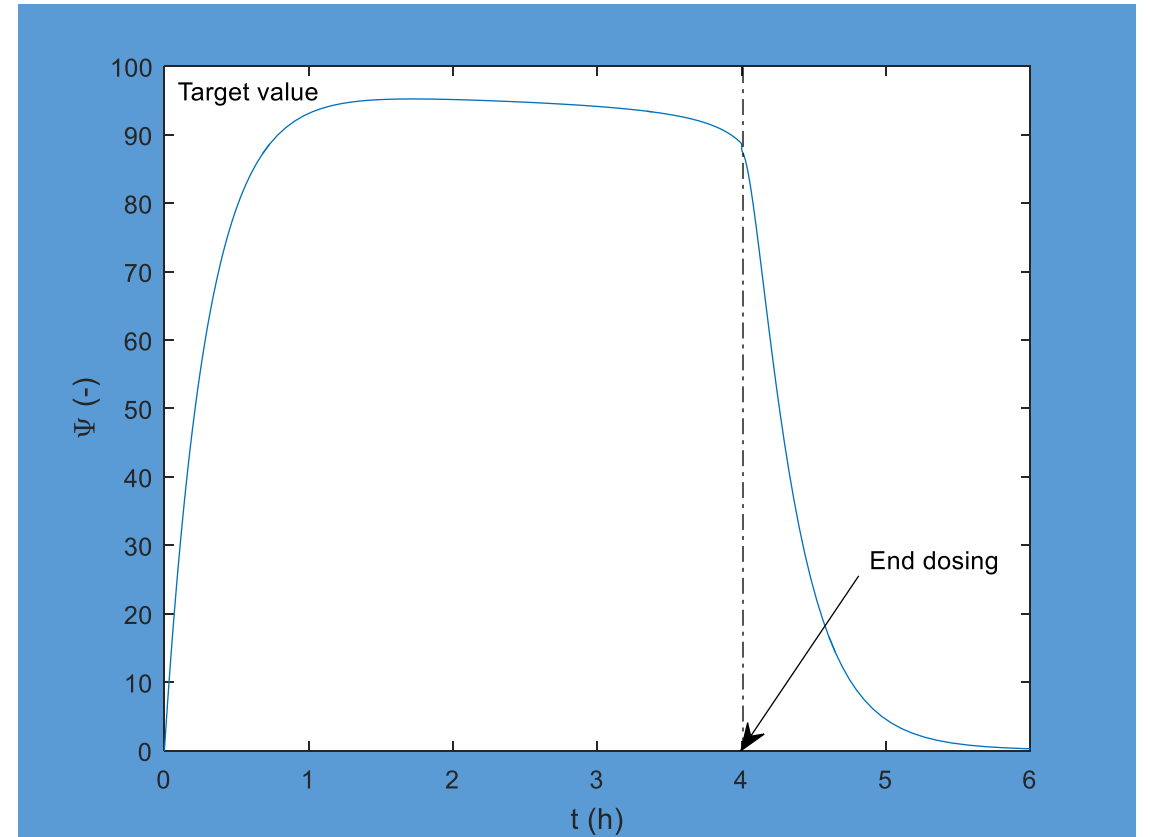
The measurement of the energy KPIs can be on-going performed during each reaction batch:

- ❖ Through available process variables (to be measured through dedicated SIL II instruments):
  - dosing stream flowrate and temperature;
  - reactor temperature;
  - external coolant flowrate and temperature increase across the jacket, coil or external heat exchangers.
- ❖ Through simple mathematical relationships;
- ❖ Knowing just the reaction enthalpy and the average specific heats of the reaction mass and the dosing stream (no kinetic characterization necessary).

# The KPIs

## $\Psi$ number

- ❖ it is the *ratio between actual and target heat removal rates*, through both the external coolant and the dosing stream;
- ❖ it is a *direct measure of the approach of the SBR operating regime to low accumulation – nearly isothermal conditions (target conditions)*;
- ❖ *under target conditions it univocally reaches values close to 100* (independently of the reaction system).

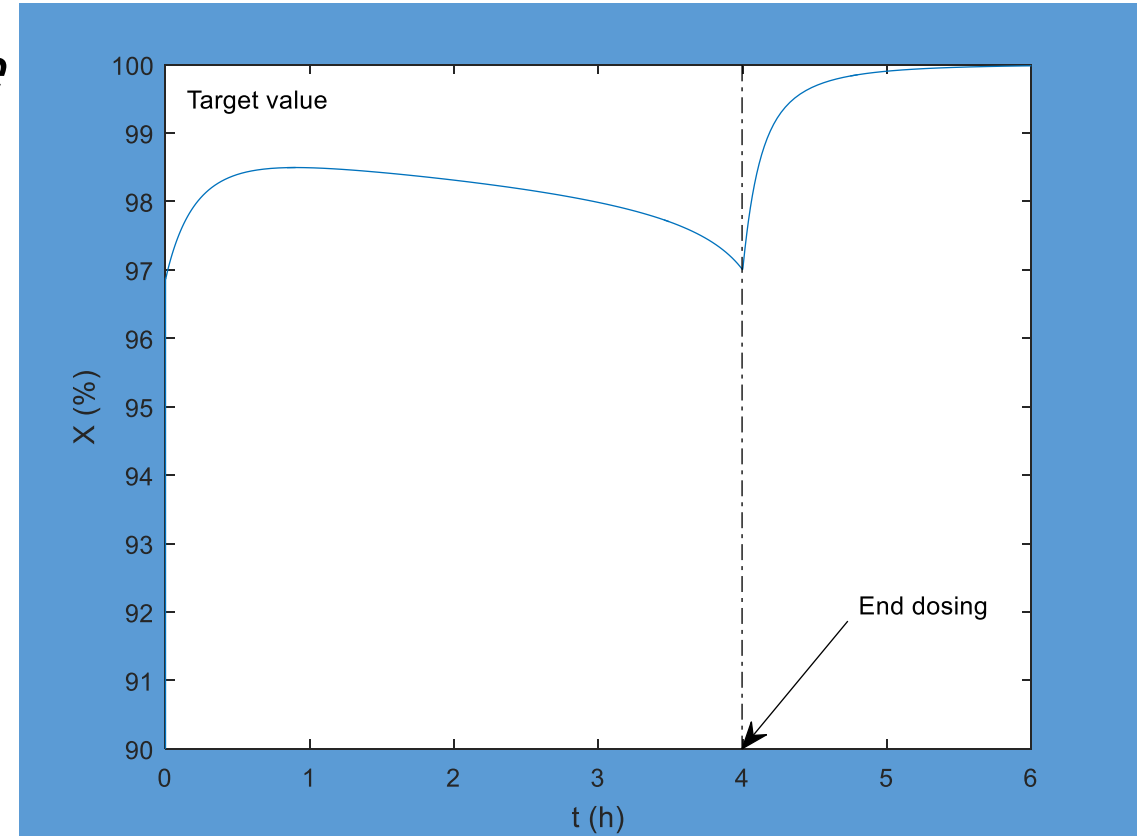




# The KPIs

## X number

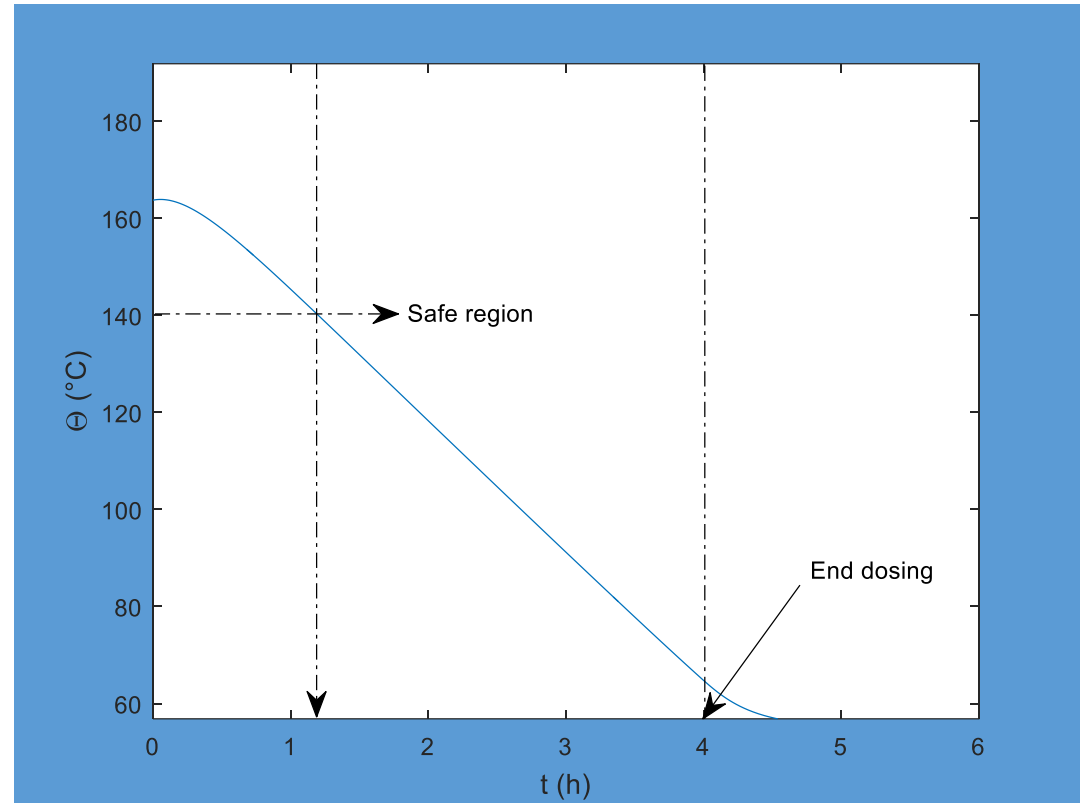
- ❖ it is the *ratio between energy sources (the reaction enthalpy) and uses (the heating enthalpy of the reaction mass and of the coolant) within the system;*
- ❖ it is a *direct measure of the conversion degree of the fed reactant (and hence of its accumulation);*
- ❖ *if at a given time all the fed reactant has been converted, X univocally reaches values close to 100 (independently of the reaction system).*



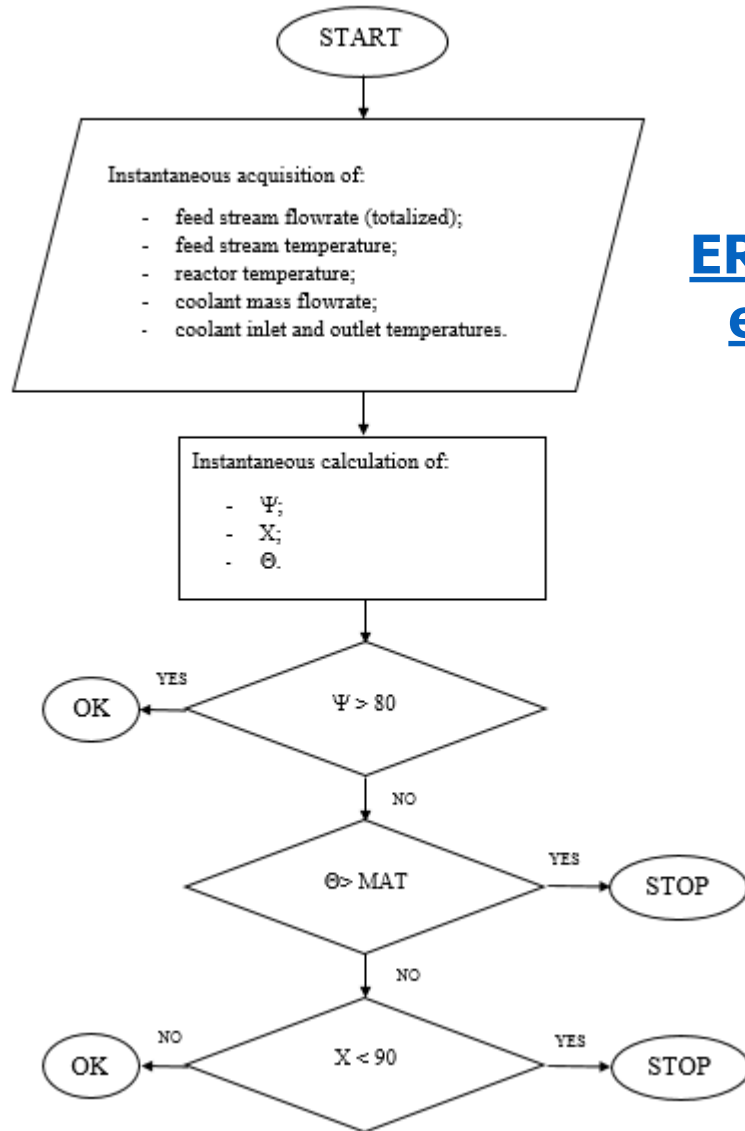
# The KPIs

## ⊕ parameter

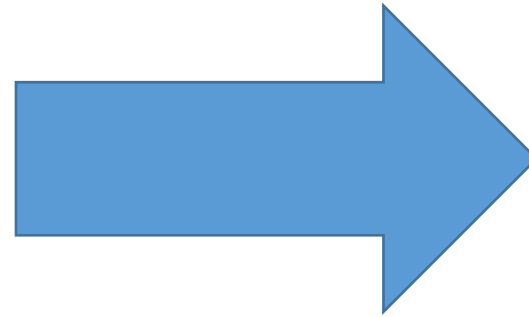
- ❖ it is the *energy potential of the system in terms of maximum attainable temperature under adiabatic conditions because of the conversion of all the reactant to be fed and of its accumulated amount;*
- ❖ *it must be compared with the maximum allowable temperature for the system (arising from safety or quality constraints).*



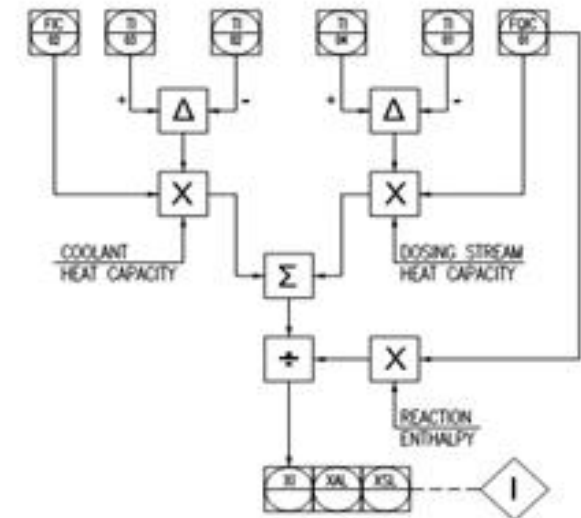
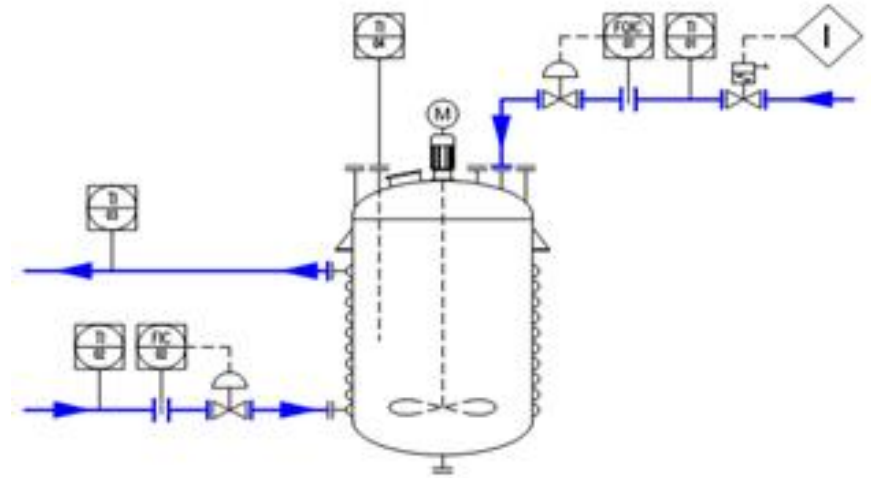
# ERMES operating logic



**ERMES allows for "seeing" the energy behavior of the SBR**



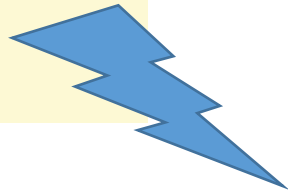
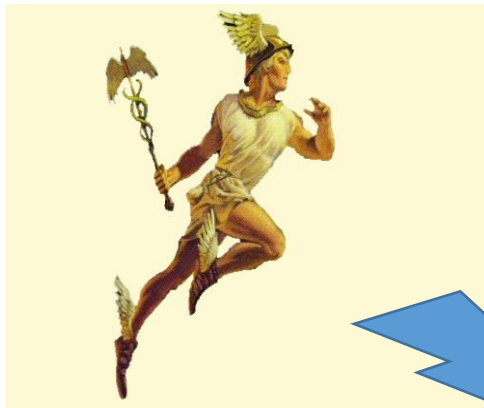
**Feed interruption without false alarms!!**



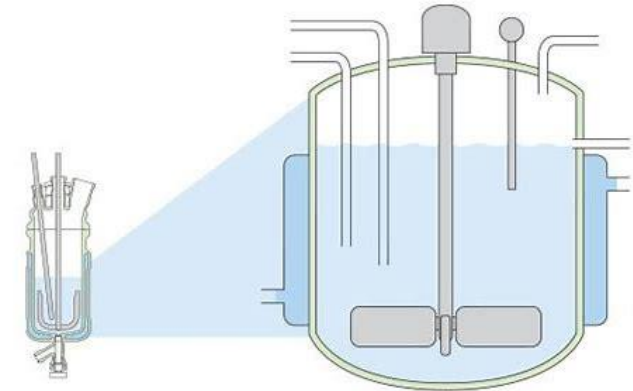
# ERMES applications

## At the lab/pilot scale

**kinetic-free setup of the safe operating conditions of the SBR**



**SAFE SCALE-UP**



$$1/U = 1/hr + dw/\lambda + 1/hj$$

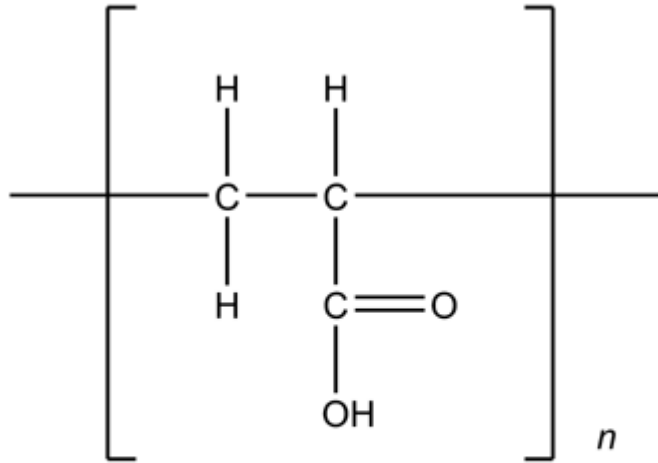
## At the industrial scale

**ERMES acts as an early messenger against unsafe scenarios  
(preventive NOT protective approach)**

# Case study: solvent based acrylic acid polymerization

## Process description

Solvent based precipitation polymerization of acrylic acid to produce crosslinked polyacrylic acids (INCI name: Carbomer®) of general formula, widely used as thickening agents for the cosmetic industry;



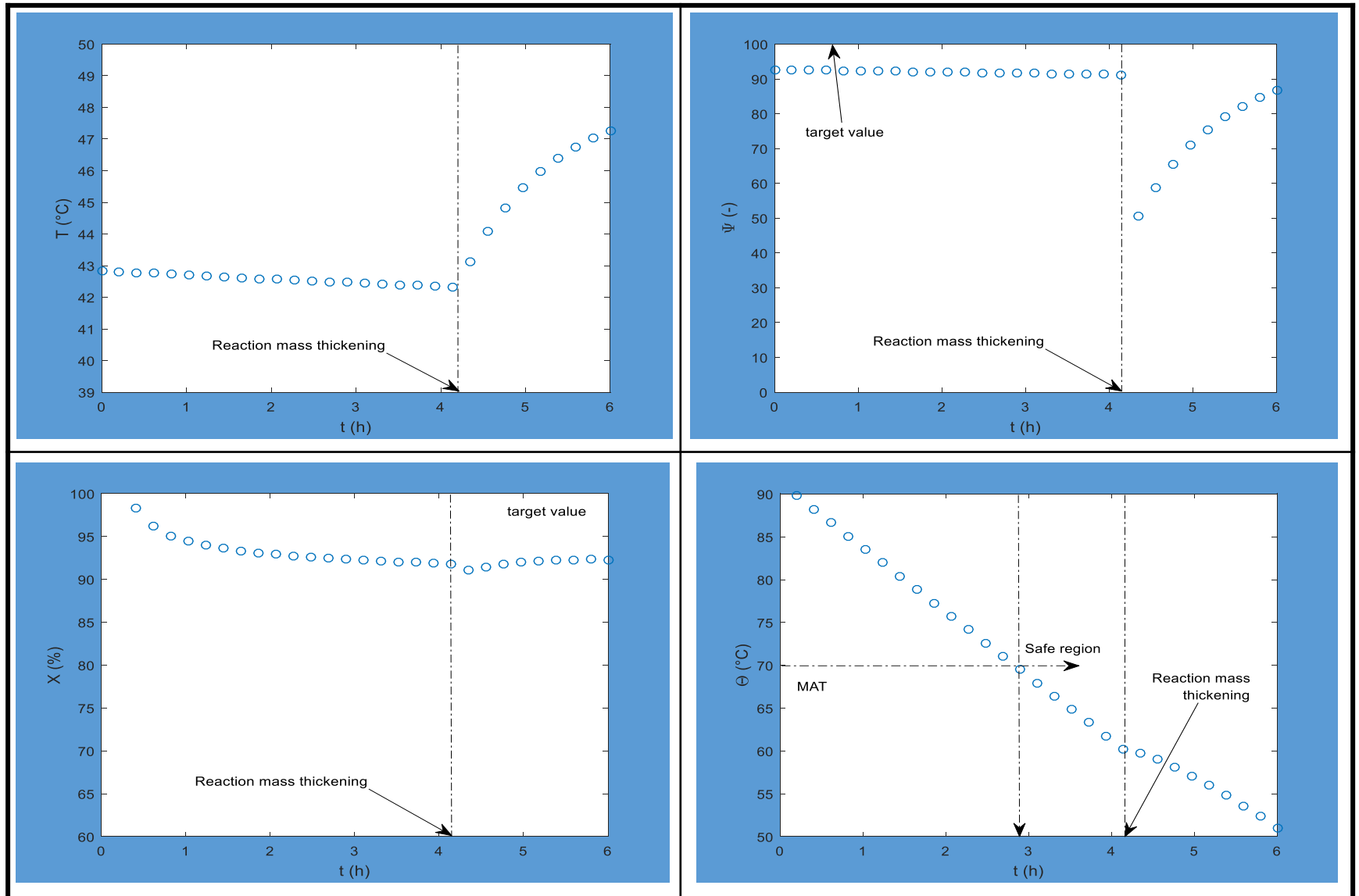
Acrylic acid monomer unit in carbomer polymers.





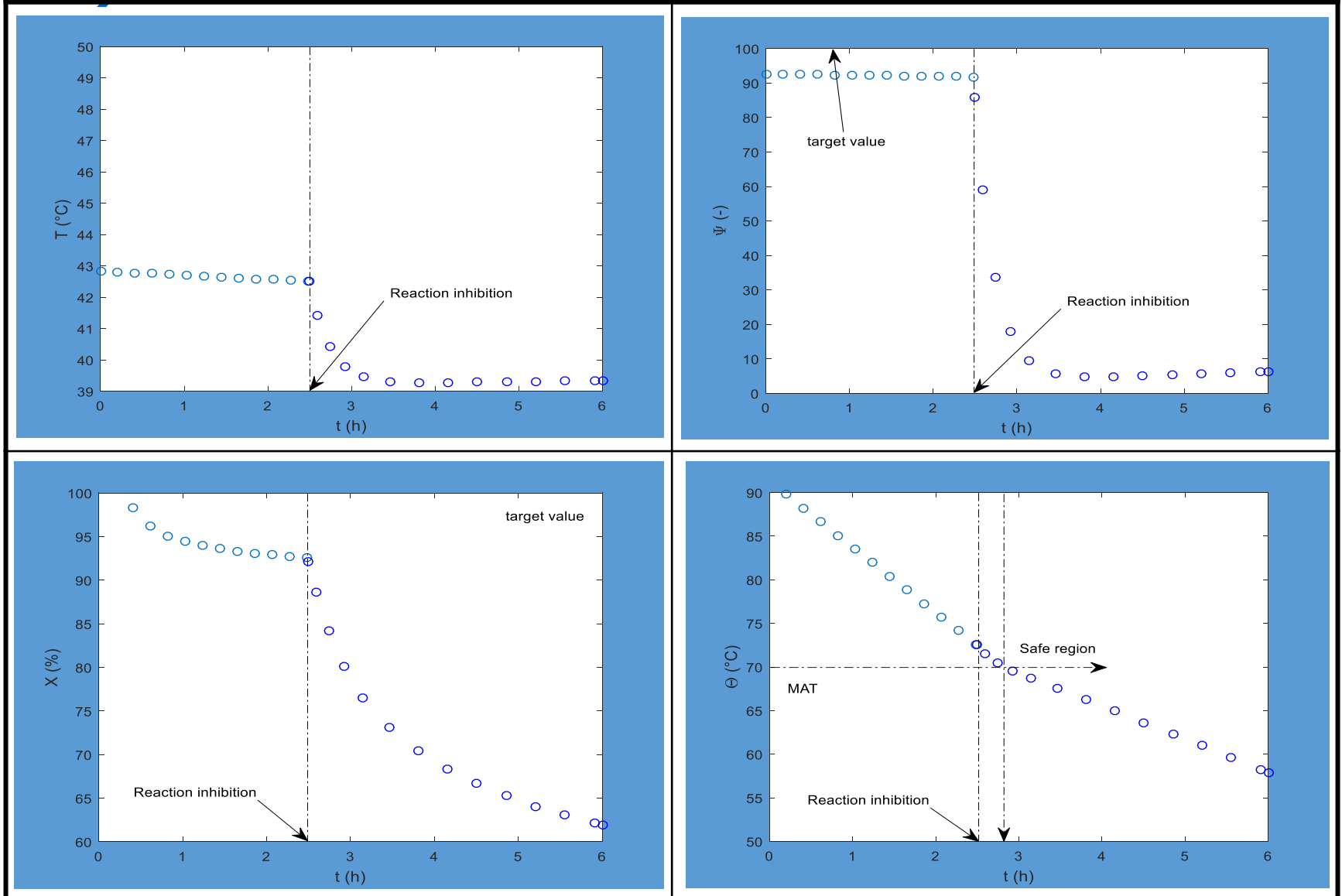
# Scenario 1): normal reaction mass thickening

**In this case only  $\Psi$  drops as a late and normal reaction thickening occurs. Therefore, the monomer feed is not interrupted.**



# Scenario 2): incidental reaction inhibition

**In this case both  $\Psi$  and  $X$  drop as an incidental reaction inhibition occurs. Therefore, the monomer feed is interrupted.**



# Final remarks

- ❖ ERMES is a useful device for significantly lowering the frequency of occurrence of incidental phenomena in SBRs, with a main focus on process safety but with a relevant saving of time and money even when facing non-catastrophic events.
- ❖ ERMES is generally useful to monitor the expected energy behavior of an exothermic semibatch reaction system, even with reference to product quality constraints.
- ❖ The installation of **ERMES cannot in any case replace a properly sized pressure relief system** (PSV or RD) on the SBR to face the worst case process scenario.
- ❖ A PCT patent application (PCT/EP2018/061657) has been filed in May 2018 about the ERMES method and related devices.