EPSC PROCESS SAFETY CONFERENCE

Vojtech MERVA

Group Head of Process & Fire Safety MOL Group

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MOLGROUP



PROCESS EVENT WITH ASSET DAMAGE FROM MOL GROUP

Date: October, 2020

A site sour water tank got damaged and released approx. 23 kg of H₂S and 800 m³ of HC+N₂ vapors to its surrounding. The event happened during the sour water manipulation and the tank's related steam purging. Fire brigade evacuated the area, and the sour water was rerouted to Sulphur Recovery unit.

Process involvement – Few hydroprocessing units at the site generate sour water that is directly processed at Claus (Sulphur recovery) units and / or temporarily stored at the particular tank.

Sour water origin – due to H_2S , NH_3 and HCl formation in hydroprocessing technologies and their mutual ammonium salt formation: $NH_3 + H_2S = NH_4HS$ a wash water has to be used that becomes a sour water, that is steam stripped.

Sour water tank -

Vertical cylindrical vessel 1400 m³ Filling at the rate of 11 m³/h Level in the tank at 40 % Temperature in the tank: 30 deg C

Brief event chronology

SW Tank's key safet

protective barriers

Sour water redirected from one hydroprocessing unit to the tank Level and pressure fluctuation in the tank Steam purging from tank to flare Pressure stabilized, level still increasing Second steam purging

Over pressurization of the tank with a consequent damage

Visual identification of the damage and gas detection H2S indication Fire brigade arrival on site and evacuation of the present people

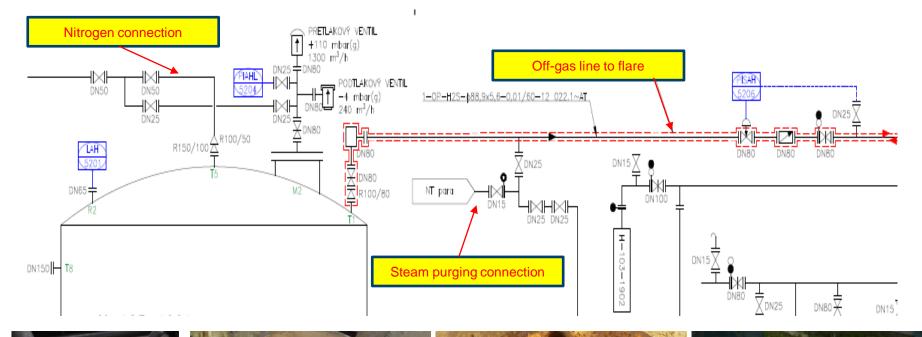
Emptying the tank and neutralization of the unpumpable material

- Over-pressure / vacuum breathing valves
- Flame arrestor
- Level indication and switch
- High pressure shut-off valve
- Nitrogen flow (purge)
- Liquid seal with ethylenglykol
- Gas detection system





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Hydro-seal valve



Upper $\mathrm{N_2}$ inlet to tank



Flange from tank to breathing valve

Block valves to breathing valve

$\rm NH_4HS$ salt formation

- As a solid substance it adds to plugging
- As a corrosive substance it adds to rust formation that further contributes to plugging

Pressure increase

- Due to the possible presence of light hydrocarbons
- Steam purging to tank and flare direction

Emergency response

1. Determination of: HOT zone: direct danger zone WARM zone: indirect danger zone COLD zone: safe zone

- 2. Considering the:
- Site survey in respect to wind direction
- Specifying measure and communication for each zones
- dividing the commanding responsibilities for each zone



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THE POSSIBLE MECHANISM OF DEFORMATION:

Initial opening (Likely the **first** place where the hoop burst), blow out direction of gaseous contents, wall extrusion, weakest place Wall bulging — counter-movement induced by movement when opened in the direction of the red arrow followed by a "vacuum"

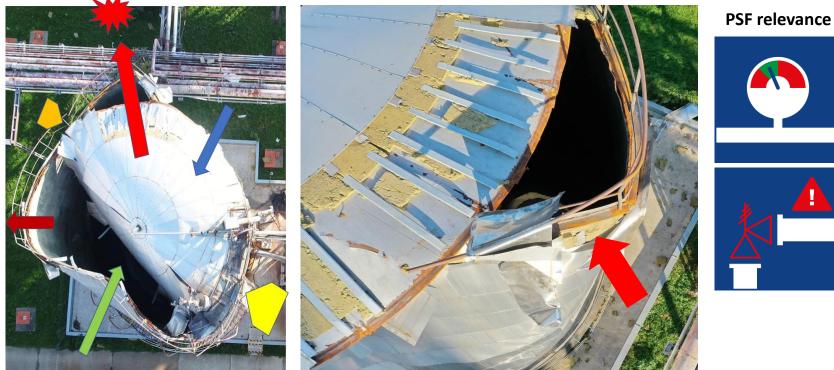
Probably just a strong reaction to the green direction. There was no debris in that direction.

vacuum this deformation could have been caused by vacuum and at the same time the roof bent inwards. Subsequently, the forces could bulge the wall in the direction of the brown arrow.

Fixed Space Narrow Width

Lessons learnt to be shared

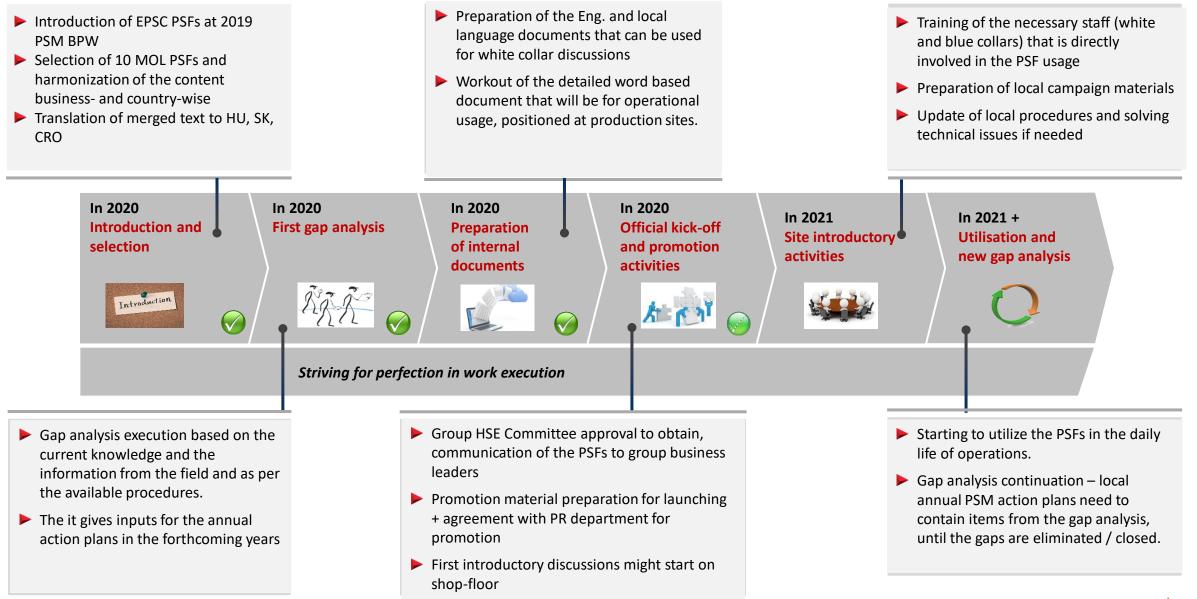
Fixed space – greater width due to stairs, firmer



- Majority of the pipelines to protective barriers have been out of function (plugged), like e.g. breathing valves and process indications
 - In sour water service, always assume the enhanced corrosion and a solid salts / sediment formation on the inner side of the tank and its equipment thus limiting its designed operation of the vessel
- **Regular inspection and cleaning** shall be performed on all safety elements in fouling service
- DCS based indications of process parameters shall routinely be cross-checked with field gauge indications
- Implement HAZOP / LOPA recommendations related to safety devices and instrumentation defined in the hazard analysis report
- Be cautious when executing purging by utilities particularly to a storage tanks
- Pay attention during SU/SD activities to use by-pass of regulation valves
- Have the **emergency response plan** always worked out for such unexpected situations and **train** them regularly



THE ACTIVITY TIMELINE OF PSF IMPLEMENTATION



THE LIST OF PROCESS SAFETY FUNDAMENTALS

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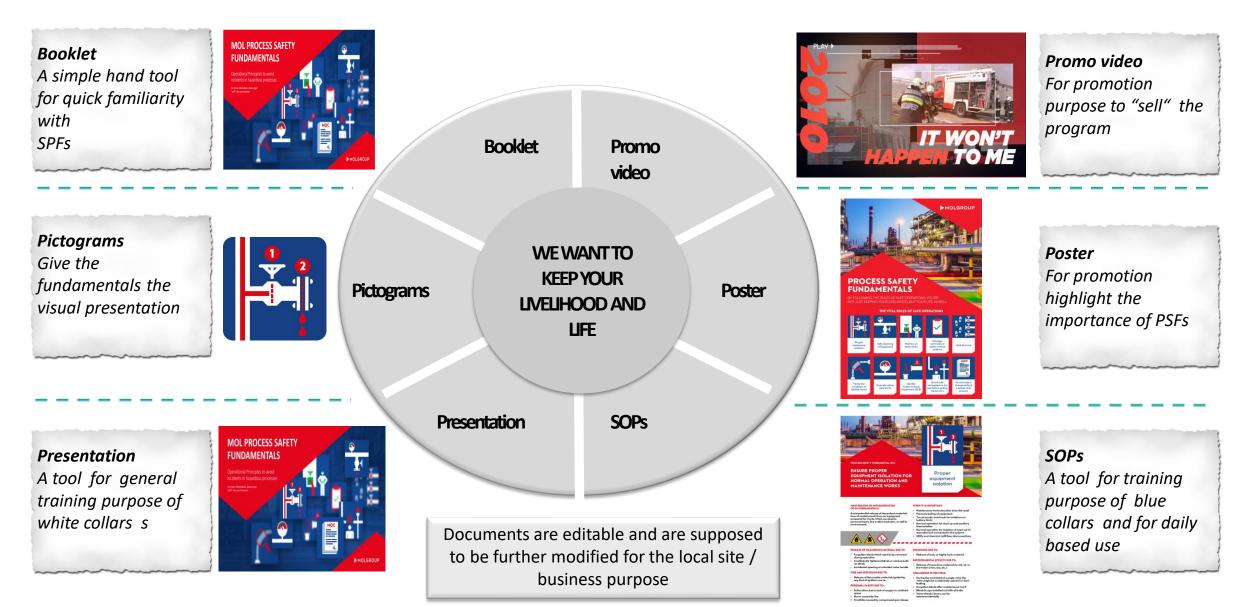
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	MOL Group PS Fundamentals		Who was targeted
	1 Ensure proper equipment isolation for normal operation and maintenance works		
EPSC listed 18 fundamentals	2 De-energize equipment before opening and reenergize it before start-up	♀ 1	
	3 Monitor an open drain	Ţ¢	
	Manage overrides and safety critical systems		***
	5 Walk the line (to ensure operational readiness vie pipeline and valve line-up)	6 6 6 7	
Selection process: via team work merging few ones from EPSC considering failures accepting business diversity targeting safety discipline	6 Verify the conditions of flexible hoses		
	7 Operate within safe limits	<u></u>	
	8 Identify safety critical equipment and report on their deficiencies	<u></u> ≱ ≜	The program is to be done in 2 phases at:
	9 Ensure safe atmosphere in the fire box before igniting the burners		REFINING & PETCHEM LOGISTICS
	10 Do not make a change without proper MoC process	Moc	ON- / OFF-SHORE UPSTREAM
	based on the work scope the full implementation is expected to last few years	1	

THE PROCESS SAFETY FUNDAMENTALS CAMPAIGN





THE PROCESS SAFETY FUNDAMENTALS FIELD IMPLEMENTATION

FROM		то	
Documents to be used	Initial and detailed gap analysis	Training of all responsibles	Utilisation
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